2.7 Petroleum Refineries

- 2.7.1 Applicability and Designation of Affected Facility
 - (a) The provisions in this source category are applicable to the following affected facilities in petroleum refineries: fluid catalytic cracking unit catalyst regenerators, fuel gas combustion devices, and all Claus sulfur recovery plants. The Claus sulfur recovery plant need not be physically located within the boundaries of a petroleum refinery to be an affected facility, provided it processes gases produced within a petroleum refinery.
 - (b) Any fluid catalytic cracking unit catalyst regenerator or fuel gas combustion device under paragraph (a) of this source category which commences construction or modification after June 11, 1973, or any Claus sulfur recovery plant under paragraph (a) of this source category which commences construction or modification after October 4, 1976 is subject to the requirements of this source category.
- 2.7.2 Test Methods and Procedures
 - In conducting the performance tests required in Section 1.2, the owner or operator shall use as (a) reference methods and procedures the test methods in Appendix A of this part or other methods and procedures as specified in this section, except as provided in §1.2(b).
 - The owner or operator shall determine compliance with the particulate matter (PM) standards in (b) **§**60.102(a)^{*} as follows:
 - (1) The emission rate (E) of PM shall be computed for each run using the following equation:

where:

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$$E = \frac{K_{C_s} Q_{sd}}{R_c}$$

- F Emission rate of PM, kg/1000 kg (lb/1000 lb) of coke burn-off. Concentration of PM, g/dscm (lb/dscf). $C_{\rm s}$
- Qsd Volumetric flow rate of effluent gas, dscm/hr (dscf/hr).
- $R_{\rm c}$ Coke burn-off rate, kg coke/hr (1000 lb coke/hr).
- Κ Conversion factor, 1.0 (kg²/g)/(1000 kg) [10³ lb/(1000 lb)]. =
- Method 5B or 5F is to be used to determine particulate matter emissions and (2) associated moisture content from affected facilities without wet FGD systems; only Method 5B is to be used after wet FGD systems. The sampling time for each run shall be at least 60 minutes, and the sampling rate shall be at least 0.015 dscm/min (0.53 dscf/min), except that shorter sampling times may be approved by the Director when process variables or other factors preclude sampling for at least 60 minutes.
- (3) The coke burn-off rate (R_c) shall be computed for each run using the following equation:

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where:

$$R_{c} = K_{I}Q_{r}(\% CO_{2} + \% CO) + K_{2}Q_{a} - K_{3}Q_{r}[(\% CO/2) + \% CO_{2} + \% O_{2}]$$

$$R_{c} = Coke \text{ burn-off rate, kg/hr (1000 lb/hr).}$$

- Or Volumetric flow rate of exhaust gas from catalyst regenerator before entering the emission control system, dscm/min (dscf/min).
- Qa Volumetric flow rate of air to FCCU regenerator, as determined from = the fluid catalytic cracking unit control room instrumentation, dscm/min (dscf/min).

- $%CO_2$ = Carbon dioxide concentration, percent by volume (dry basis).
- %CO = Carbon monoxide concentration, percent by volume (dry basis).
- $%O_2 = Oxygen concentration, percent by volume (dry basis).$
- K1 = Material balance and conversion factor, 0.2932 (kg-min)/(hr-dscm-%) [0.0186 (lb-min)/(hr-dscf-%)].
- K₂ = Material balance and conversion factor, 2.083 (kg-min)/(hr-dscm-%)[0.1303 (lb-min)/(hr-dscf-%)].
- K₃ = Material balance and conversion factor, 0.0994 (kg-min)/(hr-dscm-%) [0.0062 (lb-min)/(hr-dscf-%)].
- (i) Method 2 shall be used to determine the volumetric flow rate (Q_r).
- (ii) The emission correction factor, integrated sampling and analysis procedure of Method 3B shall be used to determine CO₂, CO, and O₂ concentrations.
- (4) Method 9 and the procedures of Section 1.3 shall be used to determine opacity.
- (c) If auxiliary liquid or solid fossil-fuels are burned in an incinerator-waste heat boiler, the owner or operator shall determine the emission rate of PM permitted in §60.102(b)[°] as follows:
 - (1) The allowable emission rate (E_s) of PM shall be computed for each run using the following equation:

$$E_s = 1.0 + A(H/R_c)K'$$

where:

- E_s = Emission rate of PM allowed, kg/1000 kg (lb/1000 lb) of coke burnoff in catalyst regenerator.
- 1.0 = Emission standard, kg coke/1000 kg (lb coke/1000 lb).
- A = Allowable incremental rate of PM emissions.
- H = Heat input rate from solid or liquid fossil fuel, million cal/hr (million Btu/hr).
- R_c = Coke burn-off rate, kg coke/hr (1000 lb coke/hr).
- K' = Conversion factor to units of standard, 1.0 $(kg^3/g)/(1000 kg)$ [10³ lb/(1000 lb)].
- (2) Procedures subject to the approval of the Director shall be used to determine the heat input rate.
- (3) The procedure in paragraph (b)(3) of this section shall be used to determine the coke burn-off rate (R_c).
- (d) The owner or operator shall determine compliance with the CO standard in §60.103(a)⁻ by using the integrated sampling technique of Method 10 to determine the CO concentration (dry basis). The sampling time for each run shall be 60 minutes.
- (e) The owner or operator shall determine compliance with the H_2S standard in \$60.104(a)(1) as follows: Method 11 shall be used to determine the H_2S concentration. The gases entering the sampling train should be at about atmospheric pressure. If the pressure in the refinery fuel gas lines is relatively high, a flow control valve may be used to reduce the pressure. If the line pressure is high enough to operate the sampling train without a vacuum pump, the pump may

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be eliminated from the sampling train. The sample shall be drawn from a point near the centroid of the fuel gas line. The sampling time and sample volume shall be at least 10 minutes and 0.010 dscm (0.35 dscf). Two samples of equal sampling times shall be taken at about 1-hour intervals. The arithmetic average of these two samples shall constitute a run. For most fuel gases, sampling times exceeding 20 minutes may result in depletion of the collection solution, although fuel gases containing low concentrations of H_2S may necessitate sampling for longer periods of time.

- (f) The owner or operator shall determine compliance with the SO₂ and the H₂S and reduced sulfur standards in \$60.104(a)(2) as follows:
 - Method 6 shall be used to determine the SO_2 concentration. The concentration in (1) mg/dscm (lb/dscf) obtained by Method 6 is multiplied by 0.3754 to obtain the concentration in ppm. The sampling point in the duct shall be the centroid of the cross section if the cross-sectional area is less than 5.00 m² (54 ft²) or at a point no closer to the walls than 1.00 m (39 in.) if the cross-sectional area is 5.00 m² or more and the centroid is more than 1 m from the wall. The sampling time and sample volume shall be at least 10 minutes and 0.010 dscm (0.35 dscf) for each sample. Eight samples of equal sampling times shall be taken at about 30-minute intervals. The arithmetic average of these eight samples shall constitute a run. Method 4 shall be used to determine the moisture content of the gases. The sampling point for Method 4 shall be adjacent to the sampling point for Method 6. The sampling time for each sample shall be equal to the time it takes for two Method 6 samples. The moisture content from this sample shall be used to correct the corresponding Method 6 samples for moisture. For documenting the oxidation efficiency of the control device for reduced sulfur compounds, Method 15 shall be used following the procedures of paragraph (f)(2) of this section.
 - (2) Method 15 shall be used to determine the reduced sulfur and H₂S concentrations. Each run shall consist of 16 samples taken over a minimum of 3 hours. The sampling point shall be the same as that described for Method 6 in paragraph (f)(1) of this section. To ensure minimum residence time for the sample inside the sample lines, the sampling rate shall be at least 3.0 lpm (0.10 cfm). The SO₂ equivalent for each run shall be calculated after being corrected for moisture and oxygen as the arithmetic average of the SO₂ equivalent for each sample during the run. Method 4 shall be used to determine the moisture content of the gases as the paragraph (f)(1) of this section. The sampling time for each sample shall be equal to the time it takes for four Method 15 samples.
 - (3) The oxygen concentration used to correct the emission rate for excess air shall be obtained by the integrated sampling and analysis procedure of Method 3B. The samples shall be taken simultaneously with the SO_2 , reduced sulfur and H_2S , or moisture samples. The SO_2 , reduced sulfur, and H_2S samples shall be corrected to zero percent excess air using the equation in paragraph (h)(3) of this section.
- (g) Each performance test conducted for the purpose of determining compliance under §60.104(b)[•] shall consist of all testing performed over a 7-day period using the applicable test methods and procedures specified in this section. To determine compliance, the arithmetic mean of the results of all the tests shall be compared with the applicable standard.
- (h) For the purpose of determining compliance with \$60.104(b)(1), the following calculation procedures shall be used:
 - (1) Calculate each 1-hour average concentration (dry, zero percent oxygen, vppm) of sulfur dioxide at both the inlet and the outlet to the add-on control device as specified in \$1.4(h). These calculations are made using the emission data collected under \$2.7.3(a).
 - (2) Calculate a 7-day average (arithmetic mean) concentration of sulfur dioxide for the inlet and for the outlet to the add-on control device using all of the 1-hour average concentration values obtained during seven successive 24-hour periods.
 - (3) Calculate the 7-day average percent reduction using the following equation:

$$R_{SO_2} = 100(C_{SO_2(i)} - C_{SO_2(o)})/C_{SO_2(i)}$$

where:

where:

- 7-day average sulfur dioxide emission reduction, percent Rso
- $C_{\text{SO}_2(i)}$ sulfur dioxide emission concentration determined in paragraph (h)(2) of this section at the inlet to the add-on control device, vppm
- sulfur dioxide emission concentration determined in paragraph Cso,(0) (h)(2) of this section at the outlet to the add-on control device, vppm
- 100 conversion factor, decimal to percent =
- (4) Outlet concentrations of sulfur dioxide from the add-on control device for compliance with the 50 vppm standard, reported on a dry, O2-free basis, shall be calculated using the procedures outlined in paragraph (h)(1) and (2) above, but for the outlet monitor only.
- (5)If supplemental sampling data are used for determining the 7-day averages under paragraph (h) of this section and such data are not hourly averages, then the value obtained for each supplemental sample shall be assumed to represent the hourly average for each hour over which the sample was obtained.
- For the purpose of adjusting pollutant concentrations to zero percent oxygen, the (6)following equation shall be used:

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$$C_{adj} = C_{meas} [20.9_c / (20.9 - \% O_2)]$$

- C_{adj} pollutant concentration adjusted to zero percent oxygen, ppm or g/dscm
- C_{meas} pollutant concentration measured on a dry basis, ppm or g/dscm =
- 20.9_c 20.9 percent oxygen-0.0 percent oxygen (defined oxygen correction basis), percent.
- 20.9 oxygen concentration in air, percent
- %O₂ = oxygen concentration measured on a dry basis, percent
- For the purpose of determining compliance with (0,104), the following reference methods (i) and calculation procedures shall be used except as provided in paragraph (i)(12) of this section:
 - One 3-hour test shall be performed each day. (1)
 - (2) For gases released to the atmosphere from the fluid catalytic cracking unit catalyst regenerator:
 - (i) Method 8 as modified in paragraph (i)(3)of this section for the concentration of sulfur oxides calculated as sulfur dioxide and moisture content,
 - (ii) Method 1 for sample and velocity traverses,
 - (iii) Method 2 calculation procedures (data obtained from Methods 3B and 8) for velocity and volumetric flow rate, and
 - (iv) Method 3B for gas analysis.
 - (3)Method 8 shall be modified by the insertion of a heated glass fiber filter between the probe and first impinger. The probe liner and glass fiber filter temperature shall be

maintained above 160°C (320°F). The isopropanol impinger shall be eliminated. Sample recovery procedures described in Method 8 for container No. 1 shall be eliminated. The heated glass fiber filter also shall be excluded; however, rinsing of all connecting glassware after the heated glass fiber filter shall be retained and included in container No. 2. Sampled volume shall be at least 1 dscm.

- For Method 3B, the integrated sampling technique shall be used. (4)
- (5) Sampling time for each run shall be at least 3 hours.
- (6) All testing shall be performed at the same location. Where the gases discharged by the fluid catalytic cracking unit catalyst regenerator pass through an incinerator-waste heat boiler in which auxiliary or supplemental gaseous, liquid, or solid fossil fuel is burned, testing shall be conducted at a point between the regenerator outlet and the incinerator-waste heat boiler. An alternative sampling location after the waste heat boiler may be used if alternative coke burn-off rate equations, and, if requested, auxiliary/supplemental fuel SO_x credits, have been submitted to and approved by the Director prior to sampling.
- (7)Coke burn-off rate shall be determined using the procedures specified under paragraph (b)(3) of this section, unless paragraph (i)(6) of this section applies.
- (8)Calculate the concentration of sulfur oxides as sulfur dioxide using equation 8-3 in Section 6.5 of Method 8 to calculate and report the total concentration of sulfur oxides as sulfur dioxide (C_{so}).
- (9) Sulfur oxides emission rate calculated as sulfur dioxide shall be determined for each test run by the following equation:

$$E_{SO_x} = C_{SO_x} Q_{sd} / 1,000$$

where:

$$E_{SO_x} = C_{SO_x} Q_{sd} / I,000$$

- Eso sulfur oxides emission rate calculated as sulfur dioxide, kg/hr
- sulfur oxides emission concentration calculated as sulfur dioxide, C_{so} = g/dscm
- dry volumetric stack gas flow rate corrected to standard conditions, Q_{sd} dscm/hr
- 1,000 = conversion factor, g to kg
- (10)Sulfur oxides emissions calculated as sulfur dioxide per 1000 kg coke burn-off in the fluid catalytic cracking unit catalyst regenerator shall be determined for each test run by the following equation:

where:

$$R_{SO_x} = E_{SO_x} / R_c$$

- R_{so} sulfur oxides emissions calculated as sulfur dioxide, kg/1,000 kg coke burn-off
- sulfur oxides emission rate calculated as sulfur dioxide, kg/hr Eso =
- R_{c} coke burn-off rate, 1,000 kg/hr =
- (11)Calculate the 7-day average sulfur oxides emission rate as sulfur dioxide per 1,000 kg of coke burn-off by dividing the sum of the individual daily rates by the number of daily rates summed.
- (12)An owner or operator may, upon approval by the Director, use an alternative method for determining compliance with (b)(2), as provided in Section 1.2(b). Any

requests for approval must include data to demonstrate to the Director that the alternative method would produce results adequate for the determination of compliance.

- (j) For the purpose of determining compliance with $(0,1)^{\circ}$, the following analytical methods and calculation procedures shall be used:
 - (1) One fresh feed sample shall be collected once per 8-hour period.
 - (2) Fresh feed samples shall be analyzed separately by using any one of the following applicable analytical test methods: ASTM D129-64 (Reapproved 1978), ASTM D1552-83, ASTM D2622-87, or ASTM D1266-87. (These methods are incorporated by reference: see §1.6.) The applicable range of some of these ASTM methods is not adequate to measure the levels of sulfur in some fresh feed samples. Dilution of samples prior to analysis with verification of the dilution ratio is acceptable upon prior approval of the Director.
 - (3) If a fresh feed sample cannot be collected at a single location, then the fresh feed sulfur content shall be determined as follows:
 - (i) Individual samples shall be collected once per 8-hour period for each separate fresh feed stream charged directly into the riser or reactor of the fluid catalytic cracking unit. For each sample location the fresh feed volumetric flow rate at the time of collecting the fresh feed sample shall be measured and recorded. The same method for measuring volumetric flow rate shall be used at all locations.
 - (ii) Each fresh feed sample shall be analyzed separately using the methods specified under paragraph (j)(2) of this section.
 - (iii) Fresh feed sulfur content shall be calculated for each 8-hour period using the following equation:

$$S_f = \sum_{i=1}^n \frac{S_i Q_i}{Q_f}$$

where:

 S_{f}

n

- fresh feed sulfur content expressed in percent by weight of fresh feed.
- number of separate fresh feed streams charged directly to the riser or reactor of the fluid catalytic cracking unit.
- Q_r = total volumetric flow rate of fresh feed charged to the fluid catalytic cracking unit.
- S_i = fresh feed sulfur content expressed in percent by weight of fresh feed for the "ith" sampling location.
- Q_i = volumetric flow rate of fresh feed stream for the "ith" sampling location.
- (4) Calculate a 7-day average (arithmetic mean) sulfur content of the fresh feed using all of the fresh feed sulfur content values obtained during seven successive 24-hour periods.
- (k) The test methods used to supplement continuous monitoring system data to meet the minimum data requirements in §60.104(d)⁻ will be used as described below or as otherwise approved by the Director.
 - (1) Methods 6, 6B, or 8 are used. The sampling location(s) are the same as those specified for the monitor.

- (2) For Method 6, the minimum sampling time is 20 minutes and the minimum sampling volume is 0.02 dscm (0.71 dscf) for each sample. Samples are taken at approximately 60-minute intervals. Each sample represents a 1-hour average. A minimum of 18 valid samples is required to obtain one valid day of data.
- (3) For Method 6B, collection of a sample representing a minimum of 18 hours is required to obtain one valid day of data.
- (4) For Method 8, the procedures as outlined in this section are used. The equivalent of 16 hours of sampling is required to obtain one valid day of data.
- 2.7.3 Monitoring of Emissions and Operations
 - (a) Continuous monitoring systems shall be installed, calibrated, maintained, and operated by the owner or operator as follows:
 - (1) For fluid catalytic cracking unit catalyst regenerators subject to \$60.102(a)(2), an instrument for continuously monitoring and recording the opacity of emissions into the atmosphere. The instrument shall be spanned at 60, 70, or 80 percent opacity.
 - (2) For fluid catalytic cracking unit catalyst regenerators subject to \$60.103(a), an instrument for continuously monitoring and recording the concentration by volume (dry basis) of CO emissions into the atmosphere, except as provided in paragraph (a)(2)(ii) of this section.
 - (i) The span value for this instrument is 1,000 ppm CO.
 - (ii) A CO continuous monitoring system need not be installed if the owner or operator demonstrates that the average CO emissions are less than 50 ppm (dry basis) and also files a written request for exemption to the Director and receives such an exemption. The demonstration shall consist of continuously monitoring CO emissions for 30 days using an instrument that shall meet the requirements of Performance Specification 4 of Appendix B of this text. The span value shall be 100 ppm CO instead of 1,000 ppm, and the relative accuracy limit shall be 10 percent of the average CO emissions or 5 ppm CO, whichever is greater. For instruments that are identical to Method 10 and employ the sample conditioning system of Method 10A, the alternative relative accuracy test procedure in \$10.1 of Performance Specification 2 may be used in place of the relative accuracy test.
 - (3) For fuel gas combustion devices subject to \$60.104(a)(1), an instrument for continuously monitoring and recording the concentration by volume (dry basis, zero percent excess air) of SO₂ emissions into the atmosphere (except where an H₂S monitor is installed under paragraph (a)(4) of this section). The monitor shall include an oxygen monitor for correcting the data for excess air.
 - (i) The span values for this monitor are 50 ppm SO_2 and 10 percent oxygen (O_2) .
 - (ii) The SO₂ monitoring level equivalent to the H₂S standard under $(0.104(a)(1))^{\circ}$ shall be 20 ppm (dry basis, zero percent excess air).
 - (iii) The performance evaluations for this SO_2 monitor under \$1.4(c) shall use Performance Specification 2. Methods 6 and 3B shall be used for conducting the relative accuracy evaluations. Method 6 samples shall be taken at a flow rate of approximately 2 liters/min. for at least 30 minutes. The relative accuracy limit shall be 20 percent or 4 ppm, whichever is greater, and the calibration drift limit shall be 5 percent of the established span value.
 - (iv) Fuel gas combustion devices having a common source of fuel gas may be monitored at only one location (i.e., after one of the combustion devices), if monitoring at this location accurately represents the SO₂ emissions into the atmosphere from each of the combustion devices.

- (4) In place of the SO₂ monitor in paragraph (a)(3) of this section, an instrument for continuously monitoring and recording the concentration (dry basis) of H₂S in fuel gases before being burned in any fuel gas combustion device.
 - (i) The span value for this instrument is $425 \text{ mg/dscm H}_2\text{S}$.
 - (ii) Fuel gas combustion devices having a common source of fuel gas may be monitored at only one location, if monitoring at this location accurately represents the concentration of H₂S in the fuel gas being burned.
 - (iii) The performance evaluations for this H_2S monitor under §1.4(c) shall use Performance Specification 7. Method 11 shall be used for conducting the relative accuracy evaluations.
- (5) For Claus sulfur recovery plants with oxidation control systems or reduction control systems followed by incineration subject to \$60.104(a)(2)(i), an instrument for continuously monitoring and recording the concentration (dry basis, zero percent excess air) of SO₂ emissions into the atmosphere. The monitor shall include an oxygen monitor for correcting the data for excess air.
 - (i) The span values for this monitor are 500 ppm SO_2 and 10 percent O_2 .
 - (ii) The performance evaluations for this SO_2 monitor under \$1.4(c) shall use Performance Specification 2. Methods 6 and 3B shall be used for conducting the relative accuracy evaluations.
- (6) For Claus sulfur recovery plants with reduction control systems not followed by incineration subject to \$60.104(a)(2)(ii), an instrument for continuously monitoring and recording the concentration of reduced sulfur and O_2 emissions into the atmosphere. The reduced sulfur emissions shall be calculated as SO_2 (dry basis, zero percent excess air).
 - (i) The span values for this monitor are 450 ppm reduced sulfur and 10 percent O_{2} .
 - (ii) The performance evaluations for this reduced sulfur (and O_2) monitor under \$1.4(c) shall use Performance Specification 5, except the calibration drift specification is 2.5 percent of the span value rather than 5 percent. Methods 15 or 15A and Method 3B shall be used for conducting the relative accuracy evaluations. If Method 3B yields O_2 concentrations below 0.25 percent during the performance specification test, the O_2 concentration may be assumed to be zero and the reduced sulfur CEMS need not include an O_2 monitor.
- (7) In place of the reduced sulfur monitor under paragraph (a)(6) of this section, an instrument using an air or O₂ dilution and oxidation system to convert the reduced sulfur to SO₂ for continuously monitoring and recording the concentration (dry basis, zero percent excess air) of the resultant SO₂. The monitor shall include an oxygen monitor for correcting the data for excess oxygen.
 - (i) The span values for this monitor are $375 \text{ ppm } SO_2$ and $10 \text{ percent } O_2$.
 - (ii) For reporting purposes, the SO₂ exceedance level for this monitor is 250 ppm (dry basis, zero percent excess air).
 - (iii) The performance evaluations for this SO₂ (and O₂) monitor under \$1.4(c) shall use Performance Specification 5. Methods 15 or 15A and Method 3B shall be used for conducting the relative accuracy evaluations.
- (8) An instrument for continuously monitoring and recording concentrations of sulfur dioxide in the gases at both the inlet and outlet of the sulfur dioxide control device from any fluid catalytic cracking unit catalyst regenerator for which the owner or operator seeks to comply with \$60.104(b)(1)[°]. The span value of the inlet monitor shall be set at 125 percent of the maximum estimated hourly potential sulfur dioxide emission

concentration entering the control device, and the span value of the outlet monitor shall be set at 50 percent of the maximum estimated hourly potential sulfur dioxide emission concentration entering the control device.

- (9) An instrument for continuously monitoring and recording concentrations of sulfur dioxide in the gases discharged into the atmosphere from any fluid catalytic cracking unit catalyst regenerator for which the owner or operator seeks to comply specifically with the 50 vppm emission limit under §60.104(b)(1)[°]. The span value of the monitor shall be set at 50 percent of the maximum hourly potential sulfur dioxide emission concentration entering the control device.
- (10) An instrument for continuously monitoring and recording concentrations of oxygen (O_2) in the gases at both the inlet and outlet of the sulfur dioxide control device (or the outlet only if specifically complying with the 50 vppm standard) from any fluid catalytic cracking unit catalyst regenerator for which the owner or operator has elected to comply with $\$60.104(b)(1)^{\circ}$. The span of this continuous monitoring system shall be set at 10 percent.
- (11) The continuous monitoring systems under paragraphs (a)(8), (a)(9) and (a)(10) of this section are operated and data recorded during all periods of operation of the affected facility including periods of startup, shutdown, or malfunction, except for continuous monitoring system breakdowns, repairs, calibration checks, and zero and span adjustments.
- (12) The owner or operator shall follow Appendix F, Procedure 1, including quarterly accuracy determinations and daily calibration drift tests, for the continuous monitoring systems under paragraphs (a)(8), (a)(9), and (a)(10) of this section.
- (13) When seeking to comply with \$60.104(b)(1)^{*}, when emission data are not obtained because of continuous monitoring system breakdowns, repairs, calibration checks and zero and span adjustments, emission data will be obtained by using one of the following methods to provide emission data for a minimum of 18 hours per day in at least 22 out of 30 rolling successive calendar days.
 - (i) The test methods as described in \$2.7.2(k);
 - (ii) A spare continuous monitoring system; or
 - (iii) Other monitoring systems as approved by the Director.
- (b) [Reserved]
- (c) The average coke burn-off rate (thousands of kilograms per hour) and hours of operation shall be recorded daily for any fluid catalytic cracking unit catalyst regenerator subject to \$60.102, \$60.103, or \$60.104(b)(2)².
- (d) For any fluid catalytic cracking unit catalyst regenerator under §60.102 that uses an incinerator-waste heat boiler to combust the exhaust gases from the catalyst regenerator, the owner or operator shall record daily the rate of combustion of liquid or solid fossil-fuels (liters/hr or kg/hr) and the hours of operation during which liquid or solid fossil-fuels are combusted in the incinerator-waste heat boiler.
- (e) For the purpose of reports under \$1.5(c), periods of excess emissions that shall be determined and reported are defined as follows:

Note: All averages, except for opacity, shall be determined as the arithmetic average of the applicable 1-hour averages, e.g., the rolling 3-hour average shall be determined as the arithmetic average of three contiguous 1-hour averages.

(1) Opacity. All 1-hour periods that contain two or more 6-minute periods during which the average opacity as measured by the continuous monitoring system under \$2.7.3(a)(1) exceeds 30 percent.

- (2) Carbon monoxide. All 1-hour periods during which the average CO concentration as measured by the CO continuous monitoring system under \$2.7.3(a)(2) exceeds 500 ppm.
- (3) Sulfur dioxide from fuel gas combustion.
 - (i) All rolling 3-hour periods during which the average concentration of SO₂ as measured by the SO₂ continuous monitoring system under \$2.7.3(a)(3) exceeds 20 ppm (dry basis, zero percent excess air); or
 - (ii) All rolling 3-hour periods during which the average concentration of H_2S as measured by the H_2S continuous monitoring system under \$2.7.3(a)(4) exceeds 230 mg/dscm (0.10 gr/dscf).
- (4) Sulfur dioxide from Claus sulfur recovery plants.
 - (i) All 12-hour periods during which the average concentration of SO₂ as measured by the SO₂ continuous monitoring system under \$2.7.3(a)(5) exceeds 250 ppm (dry basis, zero percent excess air); or
 - (ii) All 12-hour periods during which the average concentration of reduced sulfur (as SO_2) as measured by the reduced sulfur continuous monitoring system under \$2.7.3(a)(6) exceeds 300 ppm; or
 - (iii) All 12-hour periods during which the average concentration of SO₂ as measured by the SO₂ continuous monitoring system under \$2.7.3(a)(7) exceeds 250 ppm (dry basis, zero percent excess air).
- 2.7.4 Performance Test and Compliance Provisions
 - Section 1.2(d) shall apply to the initial performance test specified under paragraph (c) of this section, but not to the daily performance tests required thereafter as specified in \$60.108(d)⁻.
 Section 60.8(f) does not apply when determining compliance with the standards specified under \$60.104(b)⁻. Performance tests conducted for the purpose of determining compliance under \$60.104(b)⁻ shall be conducted according to the applicable procedures specified under \$2.7.2.
 - (b) Owners or operators who seek to comply with \$60.104(b)(3)⁻ shall meet that standard at all times, including periods of startup, shutdown, and malfunctions.
 - (c) The initial performance test shall consist of the initial 7-day average calculated for compliance with \$60.104(b)(1), (b)(2), or (b)(3)[°].
 - (d) After conducting the initial performance test prescribed under §1.2, the owner or operator of a fluid catalytic cracking unit catalyst regenerator subject to §60.104(b) shall conduct a performance test for each successive 24-hour periods thereafter. The daily performance tests shall be conducted according to the appropriate procedures specified under §2.7.2. In the event that a sample collected under §2.7.2(i) or (j) is accidentally lost or conditions occur in which one of the samples must be discontinued because of forced shutdown, failure of an irreplaceable portion of the sample train, extreme meteorological conditions, or other circumstances, beyond the owner or operators' control, compliance may be determined using available data for the 7-day period.
 - (e) Each owner or operator subject to \$60.104(b)^{*} who has demonstrated compliance with one of the provisions of \$60.104(b)^{*} but at a later date seeks to comply with another of the provisions of \$60.104(b)^{*} shall begin conducting daily performance tests as specified under paragraph (d) of this section immediately upon electing to become subject to one of the other provisions of \$60.104(b)^{*}. The owner or operator shall furnish the Director a written notification of the change in a quarterly report that must be submitted for the quarter in which the change occurred.

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de of Federal Regulations, 40CFR60, Title 40, Part 60.