

Heat Input Required to Increase Exhaust Gas Temperature for SCR Control (Recuperative" Air Heater)

Current Gas Temp	286 °F
Current Gas Temp	414.26 K
Required Gas Temp.	500 °F
Required Gas Temp.	533.15 K
Air Molecular Weight	28.967 lb/lbmol
Molal Ideal Gas (STP)	22.41 m ³ /kmol
Diameter of Stack	10.0 ft
Exit Velocity	118.8 ft/sec
Heat Capacity Constant a	28.09
Heat Capacity Constant b	1.97E-03
Heat Capacity Constant c	4.80E-06
Heat Capacity Constant d	-1.97E-09

Heat Capacity of Air ¹

$$C_p \text{ (J/mol} \cdot \text{K)} = a + bT + cT^2 + dT^3$$

$$= 2.96E+01 \text{ @ } 500 \text{ }^{\circ}\text{F}$$

$$3.02E+01 \text{ @ } 650 \text{ }^{\circ}\text{F}$$

Volumetric Flow Rate

$$\text{Volumetric Flow Rate} = (\pi \times D^2/4) \times \text{exit velocity} \times 3600 \text{ sec/hr}$$

$$= 33,589,909 \text{ ft}^3/\text{hr}$$

$$= 951,160 \text{ m}^3/\text{hr}$$

Convert Volumetric Flow Rate to Molar Flow Rate

$$\text{Molar Flow Rate} = \text{Volumetric Flow Rate (m}^3/\text{hr)} \times (1/\text{molal ideal gas, at STP}) \times \text{Temperature Conversion}$$

$$= 30,020 \text{ kmol/hr}$$

$$30,019,709 \text{ mol/hr}$$

Calculate Heat Input Required

$$\text{Heat Input} = \text{Molar Flow Rate} \times (\Delta T \text{ K}) \times \text{Average Heat Capacity over Temp. Range}$$

$$= 106,699,844,000 \text{ J/hr}$$

$$= 101,199,467 \text{ Btu/hr}$$

$$140,554,815 \text{ Btu/hr (corrected for efficiency of boiler}$$

$$\text{ - 72\% per Mark Sajer 10 Apr 08)}$$

$$165,358,606 \text{ Btu/hr (corrected for efficiency of air heater}$$

$$\text{ - 85\% per Mark Sajer 10 Apr 08)}$$

Notes:

¹ Elementary Principles of Chemical Process, 1986

Heat Input Required to Increase Exhaust Gas Temperature for SCR Control (Duct Burner)

Current Gas Temp	500 °F
Current Gas Temp	533.15 K
Required Gas Temp.	650 °F
Required Gas Temp.	616.48 K
Air Molecular Weight	28.967 lb/lbmol
Molal Ideal Gas (STP)	22.41 m ³ /kmol
Diameter of Stack	10.0 ft
Exit Velocity	118.8 ft/sec
Heat Capacity Constant a	28.09
Heat Capacity Constant b	1.97E-03
Heat Capacity Constant c	4.80E-06
Heat Capacity Constant d	-1.97E-09

Heat Capacity of Air ¹

$$\begin{aligned}C_p \text{ (J/mol} \cdot \text{K)} &= a + bT + cT^2 + dT^3 \\&= 3.02\text{E}+01 \text{ @ } 500 \text{ }^\circ\text{F} \\&= 3.07\text{E}+01 \text{ @ } 650 \text{ }^\circ\text{F}\end{aligned}$$

Volumetric Flow Rate

$$\begin{aligned}\text{Volumetric Flow Rate} &= (\pi \times D^2/4) \times \text{exit velocity} \times 3600 \text{ sec/hr} \\&= 33,589,909 \text{ ft}^3/\text{hr} \\&= 951,160 \text{ m}^3/\text{hr}\end{aligned}$$

Convert Volumetric Flow Rate to Molar Flow Rate

$$\begin{aligned}\text{Molar Flow Rate} &= \text{Volumetric Flow Rate (m}^3/\text{hr)} \times (1/\text{molal ideal gas, at STP}) \times \text{Temperature Conversion} \\&= 23,325 \text{ kmol/hr} \\&= 23,325,452 \text{ mol/hr}\end{aligned}$$

Calculate Heat Input Required

$$\begin{aligned}\text{Heat Input} &= \text{Molar Flow Rate} \times (\Delta T \text{ K}) \times \text{Average Heat Capacity over Temp. Range} \\&= 59,155,652,011 \text{ J/hr} \\&= 56,106,178 \text{ Btu/hr}\end{aligned}$$

$$59,500,000 \text{ Btu/hr}$$

Burns & Roe estimate 10 Apr 08

Notes:

¹ Elementary Principles of Chemical Process, 1986